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Research Article

Synergistic co-pyrolysis of *Gracilaria* waste and waste tires: Enhancing bio-oil quality through thermal and chemical bond optimization

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Abstract. The increasing demand for renewable energy and sustainable waste management has prompted research into innovative conversion technologies. This study explored the co-pyrolysis of Gracilaria waste (GW) and waste tires (WT) as a potential approach to improving bio-oil quality by enhancing its hydrocarbon content and reducing oxygenated compounds. The novelty of this study lay in providing new mechanistic insights into the co-pyrolysis process by systematically analyzing the thermal degradation behavior and chemical bond evolution of GW-WT mixtures using a combination of TGA, FTIR, and GC-MS techniques. This detailed chemical transformation analysis differentiated the study from prior research that primarily focused on product yields. The study analyzed the thermal degradation behavior and chemical bond transformation of GW and WT mixtures during pyrolysis, hypothesizing that the addition of WT to GW would enhance the hydrocarbon profile and thermal stability of the resulting bio-oil. Thermogravimetric analysis (TGA) was employed to evaluate the decomposition behavior of five different GW-WT blend ratios under an inert atmosphere, while Fourier Transform Infrared Spectrosco py (FTIR) was used to assess chemical functional group evolution in both raw materials and pyrolytic products. The results revealed that GW pyrolysis exhibited a single weight loss peak (100-350°C) with a total weight loss of 40%, while WT pyrolysis followed a two-stage decomposition process (200-500°C) with a total weight loss of 65%. The GW-WT mixture resulted in a total weight loss of approximately 60%, indicating a synergistic effect between the two feedstocks. FTIR analysis confirmed a reduction in hydroxyl (-OH) groups and an increase in hydrocarbon-related bonds (C=C, C-C, and C-H), demonstrating improved bio-oil composition. These findings suggested that incorporating waste tires into Gracilaria pyrolysis enhanced bio-oil quality and hydrocarbon content, offering a promising approach for biomass valorization and sustainable energy production. Future research should explore process optimization through catalyst integration and scale-up potential for industrial applications.

Keywords: co-pyrolysis, Gracilaria waste, waste tires, thermal degradation, chemical bonds shift



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1. Introduction

The escalating global energy demand, driven by industrialization and population growth, necessitates the transition from fossil fuels to more sustainable energy sources. Fossil fuel dependence contributes significantly to greenhouse gas emissions, exacerbating environmental concerns such as global warming and climate change. Additionally, the depletion of conventional energy reserves highlights the urgency of adopting renewable alternatives. Biomass has emerged as a promising renewable energy source due to its carbon-neutral nature and widespread availability. Among various biomass sources, marine-derived biomass waste, particularly the byproducts of the agar industry, presents a viable feedstock for energy production. Gracilaria, a red seaweed abundantly found in Indonesian waters and commonly used for agar production,

can be converted into valuable biofuels through thermochemical processes such as pyrolysis (Amrullah *et al.*, 2023; Farobie *et al.*, 2024).

Pyrolysis, a thermochemical decomposition process under inert conditions, has gained attention for converting biomass into liquid bio-oil, gaseous fuels, and solid char (Ma *et al.*, 2023). This process plays a crucial role in sustainable waste management while providing a renewable energy source (Chen *et al.*, 2023; Prasetiawan *et al.*, 2024)). Additionally, bio-oil derived from pyrolysis, commonly referred to as pyrolytic oil or bio-crude oil, is a complex mixture of organic compounds with potential applications in energy and chemical industries (Masfuri *et al.*, 2024). Solid waste management is another critical challenge, particularly concerning the disposal of waste tires, which accumulate in massive quantities, with approximately 300 million discarded annually worldwide (Li *et al.*, 2023). As a

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carbonaceous solid waste, waste tires possess high energy content and hydrocarbon composition, making them a promising feedstock for pyrolysis (Mavukwana *et al.*, 2021). Conventional landfill disposal poses severe environmental risks, necessitating the development of environmentally friendly disposal techniques (Wang *et al.*, 2023b). Pyrolysis of waste tires offers an efficient solution by transforming them into valuable energy products while mitigating environmental pollution (Alzahrani *et al.*, 2025; F. Wang *et al.*, 2022). The co-pyrolysis of biomass with plastic waste, such as polyethylene terephthalate (PET), has been studied to enhance bio-oil yield and improve fuel quality (Amrullah *et al.*, 2024).

Given their high carbon content and energy potential, waste tires have been identified as an effective co-pyrolytic reactant when combined with biomass. Co-pyrolysis, which involves the simultaneous thermal degradation of multiple feedstocks, enhances the quality of pyrolysis products due to synergistic interactions (Abnisa & Wan Daud, 2014). Researchers have demonstrated that co-pyrolysis improves the yield and quality of bio-oil by optimizing the hydrogen-to-carbon ratio (Zhang et al., 2024). Waste tires and biomass co-pyrolysis has been investigated with various feedstocks, including wood biomass and polyethylene, with results indicating improved liquid fuel production (Hussain et al., 2021; Martínez et al., 2014b). The interaction between biomass and rubber-derived compounds further contributes to the complexity and diversity of the pyrolysis liquid, which contains a range of valuable chemicals such as acids, ketones, phenols, and aromatics (González et al., 2010; Kim, 2015). The thermochemical conversion of macroalgae such as Ulva lactuca, Padina sp. has also been explored, with studies showing the potential of marine biomass for producing biofuels with reduced oxygenated compounds and enhanced hydrocarbon content when combined with waste plastics (Amrullah et al., 2022; Farobie et al., 2024).

To comprehensively analyze the thermal degradation behavior and chemical transformations occurring during pyrolysis. advanced analytical techniques such thermogravimetric analysis (TGA) and Fourier Transform Infrared Spectroscopy (FTIR) are widely employed. TGA provides critical insights into mass loss and decomposition kinetics, while FTIR identifies chemical functional group evolution during pyrolysis (Liang et al., 2019). The combination of TG-FTIR-MS techniques has proven effective in analyzing the co-pyrolysis of various materials, including corn stover and high-density polyethylene (Kai et al., 2017), as well as waste tires (Januszewicz et al., 2017). These techniques facilitate a detailed understanding of pyrolysis reaction mechanisms, particularly in terms of shifting chemical bonds and decomposition pathways under different thermal conditions (Idris et al., 2010; Vuthaluru, 2004). Recent studies have further optimized the bio-oil yield and quality using response surface methodology (RSM), indicating that precise control of temperature and feedstock ratios can significantly enhance fuel properties (Amrullah et al.,

Although significant research has been conducted on biomass and waste tire pyrolysis—such as the works of Martínez et al. (2014c), Tang et al. (2019), and Alvarez et al. (2019), which primarily focused on product yields and general compositional trends—studies providing detailed mechanistic insights into the thermal degradation behavior and chemical bond evolution of biomass—tire mixtures remain scarce. This study specifically addresses this gap by employing combined TGA, FTIR, and GC-MS analyses to elucidate how varying GW-WT ratios influence decomposition pathways and chemical

structure transformations, offering a deeper understanding of synergistic interactions in the co-pyrolysis process.

2. Material and Methods

2.1 Sample Preparation

Seaweed waste from Gracilaria (GW) and waste tires (WT) were used as feedstocks for the experimental runs. The Gracilaria waste was obtained from the seaweed home industry, Rumput Laut Mandiri, in Wonosari, Gunung Kidul, Jogjakarta. The seaweed was harvested and processed during the 2023 season, and the residual waste from agar extraction was utilized as feedstock for this study. The waste tires were pre-shredded to a particle size of under 20 mesh. The Gracilaria waste was initially milled and sieved using a 20-mesh screen to obtain fine particles before being dried in an oven at 105°C for 6 hours. The dried samples were then stored in an airtight container to prevent moisture absorption. The GW and WT feedstocks were mixed at mass ratios of 100/0, 75/25, 50/50, 25/75, and 0/100 (w/w) for subsequent experimental procedures.

2.2 Thermogravimetric Analysis (TGA)

Thermal degradation analysis was conducted using a thermogravimetric analyzer (TGA 701, LECO, Model No. 604-100-700) to determine the degradation temperatures, thermal behavior, and theoretical volatility of the samples under an inert nitrogen (N₂) atmosphere. A sample weighing 8.0 mg was placed in an aluminum crucible and heated from room temperature to 700°C at a heating rate of 20°C/min under a constant N_2 flow rate of 20 mL/min. The results from the TGA analysis served as the basis for determining the experimental pyrolysis temperature range.

2.3 Fourier Transform Infrared Spectroscopy (FTIR)

Fourier transform infrared (FTIR) spectroscopy was performed to analyze the spectral characteristics of both the raw materials and the liquid pyrolytic products. The analysis was conducted using an FTIR spectrometer (Bruker-Tensor II) equipped with an attenuated total reflectance (ATR) accessory and a ZnSe/Zinc Selenide beam splitter. FTIR was employed to identify the functional groups present in the feedstocks before pyrolysis and in the liquid products after pyrolysis. Infrared spectra were recorded with a resolution of 4.0 cm⁻¹ over a wavenumber range of 4000–500 cm⁻¹.

2.4 Gas Chromatography-Mass Spectrometry (GC-MS)

analytical technique was conducted using gas chromatography mass spectrometry (GC-MS) to perform detailed chemical characterization of bio-oil components. The chromatographic analysis of the liquid fraction was carried out on an Agilent chromatograph equipped with an Agilent-MS mass spectrometer. The separation was performed on an HP-DMS capillary column (30 mm \times 0.25 mm ID \times 0.25 μ m) at an initial temperature of 50°C, which was maintained for 10 minutes at the final temperature. A 0.5 µL aliquot of the sample was injected for analysis. The identification of compounds was conducted based on a comparison with the NIST library database, using a similarity threshold above 60%. The results were reported in a semi-quantitative manner, based on the relative peak areas in the total ion chromatogram (TIC). No internal standards were used in this analysis. The peak area percentages thus reflect the approximate abundance of each

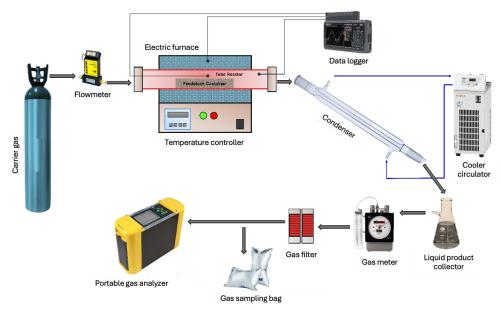


Fig. 1 Schematic diagram of the co-pyrolysis experimental setup

compound relative to the total detected compounds in the sample.

2.5 Pyrolysis Experimental Procedure

The pyrolysis experiments were carried out at atmospheric pressure in a horizontal stainless steel tubular reactor with an inner diameter of 5 cm, an outer diameter of 5.6 cm, and a length of 40 cm. The experimental setup included an N_2 supply, flow meter, tubular pyrolysis reactor, electrically heated furnace with a proportional-integral-derivative (PID) temperature controller, condenser, liquid collection unit, gas meter, gas sampling system, gas filter, and gas analyzer (Figure 1).

3. Results and Discussion

3.1 Thermogravimetric Analysis

The thermogravimetric analysis (TGA) revealed significant thermal decomposition patterns and corresponding reaction rates. Figure 2 presents the TG curves for the five sample mixtures at a heating rate of 20°C/min. The thermogravimetric analysis (TGA) plot elucidates the thermal decomposition behavior of materials with varying compositions, specifically labeled as GW and WT. The TGA results typically reveal weight loss occurring in three distinct stages: the initial release of moisture and volatiles (approximately 0-150°C), followed by primary degradation (150-450°C), and concluding with a stabilization phase (450-700°C). This pattern is consistent with findings in the literature, where TGA has been employed to analyze the thermal stability of various composite materials, indicating that the initial weight loss is often attributed to moisture and volatile components (Xu et al., 2019; Zabihzadeh, 2010). In the context of the GW100+WT0 sample, which demonstrates the highest thermal stability, it is noted that this composition exhibits a slower degradation rate and retains a greater residual weight at elevated temperatures. This observation aligns with studies that have shown how specific material compositions can significantly influence thermal stability and degradation rates. For instance, Zabihzadeh discusses the importance of thermal stability in composite materials, highlighting how variations in composition can lead

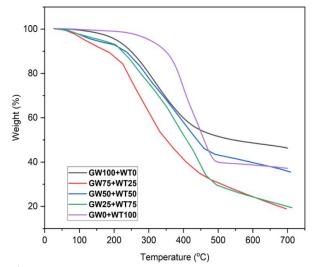


Fig. 2 Thermogravimetry analysis (TGA) curve of Gracilaria (GW), waste tires (WT), and both mixture

to different thermal behaviors (Zabihzadeh, 2010). Similarly, Xu et al. (2019) emphasize the role of material composition in determining the thermal degradation characteristics of composites, supporting the assertion that GW enhances thermal stability. Conversely, the GW0+WT100 sample, which is rich in WT, exhibits lower thermal resistance, characterized by an earlier onset of decomposition and reduced char formation. This phenomenon suggests that increased WT content may compromise the structural integrity of the material, leading to more rapid degradation. The literature supports this observation, as studies have indicated that the presence of certain components can adversely affect the thermal stability of composites. For example, Khalil et al. (2022) noted that the thermal stability of composites can be influenced by their constituent materials, which can lead to variations in degradation rates and char yield. Furthermore, the kinetic studies on thermal decomposition have shown that the composition of the materials plays a crucial role in determining their thermal behavior, as evidenced by the findings of Islam

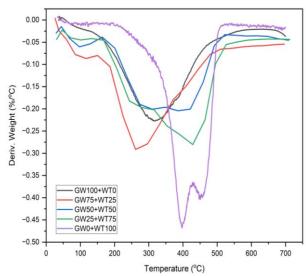


Fig. 3 Derivative Thermogravimetry (DTG) curve of Gracilaria (GW), waste tires (WT), and both mixture

and Gafur (2023), who explored the thermal properties of various composite materials.

Figure 3 shows the Derivative Thermogravimetric (DTG) curve, which represents the rate of weight loss (derivative weight, %/°C) as a function of temperature. The DTG curves obtained from thermogravimetric analysis provide critical insights into the thermal degradation behavior of various samples, particularly in relation to their composition of green waste (GW) and wood waste (WT). The distinct peaks observed in the DTG curves correspond to the maximum degradation rates of the samples, indicating the temperatures at which decomposition occurs most rapidly.

The initial broad peaks in the range of 100-200 °C are primarily attributed to moisture evaporation and the release of low-molecular-weight volatiles. This phenomenon has been documented in studies examining the thermal behavior of natural polymers and composites (Bakirtzis et al., 2014). For instance, Bakirtzis et al. noted that the addition of fire retardants to lignocellulosic materials resulted in a shift of decomposition profiles towards lower temperatures, which aligns with the observed behavior in the current analysis (Bakirtzis et al., 2014). The major decomposition peaks, occurring between 250-500°C, represent the thermal degradation of organic components. Variations in peak temperature and intensity are influenced by the GW and WT composition. Specifically, the GW100+WT0 sample exhibits a relatively higher peak temperature, suggesting enhanced thermal stability, while the GW0+WT100 sample shows a more intense and lowertemperature degradation peak, indicating reduced thermal resistance. This observation is consistent with findings by Yang et al., who demonstrated that the thermal stability of materials is significantly influenced by their composition and structure (Yang et al., 2017). Furthermore, the results corroborate the work of Çulhaoğlu and Kaya (2015), who highlighted the importance of material composition in determining thermal stability and degradation characteristics. As the WT content increases, the decomposition shifts to lower temperatures, accompanied by sharper peaks that imply a faster degradation rate. This trend suggests that higher WT content compromises thermal stability, a conclusion supported by research indicating that the presence of certain components can accelerate thermal breakdown (Huang et al., 2014). For example, Huang et al. (2014) discussed how the thermal stability of phase change

materials can be affected by their composition, leading to variations in degradation behavior. Additionally, the residual stability observed above 500°C indicates differences in char formation, with GW-rich samples retaining more thermally stable residues. This finding aligns with the work of Rybiński and Janowska, who emphasized the significance of char formation in enhancing thermal stability (Rybiński & Janowska, 2014).

3.2 Fourier Transform Infrared (FTIR)

Thermal The FTIR spectrum of the raw materials is depicted in Figure 4, illustrating the absorption of infrared radiation at various wavelengths. The extent of light absorption at a given wavelength determines the transmittance level, where stronger absorption peaks correspond to lower transmittance values (Z. Wang et al., 2023a). The black spectrum represents Gracilaria waste (GW) as the raw material. The peak observed between 3500 and 3700 cm⁻¹ is associated with free -OH groups, indicating the presence of alcohol, water, and phenolic compounds (Mecozzi & Sturchio, 2017). The peak at 2981 cm⁻¹ corresponds to C-H ring stretching in aromatic groups, while the peaks at 2876 cm⁻¹ and 2822 cm⁻¹ are linked to C-H bonds in alkanes and aldehydes, respectively. The presence of alkanes is further verified by the C-H vibrations occurring within the 3000-2800 cm⁻¹ range. Additionally, the peaks at 2357 and 2332 cm⁻¹ correspond to C=O and N=C=O bonds in hemicellulose, confirming the presence of aldehydes, ketones, and carbonyl groups. The peak at 2294 cm⁻¹ represents C≡N stretching of nitriles, while the band between 2260 and 2210 cm⁻¹ further verifies the presence of nitrile groups. The peaks at 1055 and 1033 cm⁻¹ indicate C-O stretching in alcohol compounds, whereas those at 1008 and 875 cm⁻¹ correspond to C=C bonds in benzene and alkenes. The identification of OH as H2O and CO suggests the release of oxygen during the pyrolysis process. The formation of H₂O primarily results from hydroxyl dehydration reactions associated with cellulose hemicellulose in the algal biomass. Meanwhile, the production of alcohols, aldehydes, and ketones is mainly driven by the pyrolytic breakdown of cellulose and hemicellulose.

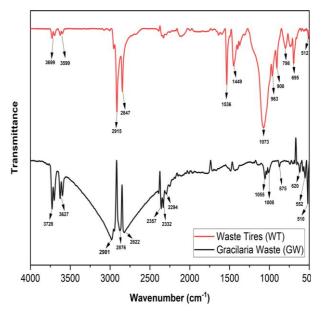


Fig. 4 FTIR Spectrum of raw materials of GW and WT

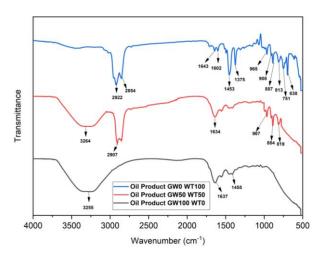


Fig. 5 FTIR spectrum of liquid products

Figure 5 show the FTIR spectra of the chemical composition of oil products derived from varying ratios of Gracilaria waste (GW) and waste tires (WT). The black spectrum (GW100+WT0), which represents 100% Gracilaria waste, reveals a broad O-H stretching peak at 3265 cm-1. This peak indicates the presence of hydroxyl groups, likely from alcohols or water, and is consistent with findings from previous studies that have identified similar functional groups in biomass-derived oils (Forero-Doria et al., 2015). The strong C=O stretching observed at 1637 cm⁻¹ suggests the presence of aldehydes, ketones, or carboxyl compounds resulting from biomass decomposition, which aligns with the thermal degradation characteristics reported in the literature (Puri et al., 2024). In contrast, the blue spectrum (GW0+WT100), derived solely from waste tires, exhibits peaks at 2924 cm⁻¹ and 2852 cm⁻¹, corresponding to C-H stretching vibrations typical of alkanes. The multiple peaks in the fingerprint region (1025, 975, 913, 833, and 754 cm⁻¹) signify the presence of aromatic and aliphatic hydrocarbons, which are characteristic of tire pyrolysis products (Bakirtzis et al., 2014). This observation is supported by the work of Onay, who discussed the chemical composition of pyrolysis products from waste tires, highlighting the prevalence of hydrocarbon structures (Onay, 2014). The red spectrum (GW50+WT50), obtained from an equal mixture of GW and WT, illustrates a blend of both biomass and tire-derived compounds, indicating the complexity of the chemical interactions during co-pyrolysis. These spectral characteristics

correspond to functional bonds and wavenumber ranges identified in FTIR spectroscopy, as detailed in the Table 1.

To provide a more quantitative perspective on the FTIR results, we analyzed the relative intensity changes of key characteristic bands across different GW-WT mixtures. The intensities of the hydroxyl (-OH) stretching band (~3265 cm⁻¹), carbonyl (C=O) stretching band (~1637 cm⁻¹), and aromatic C=C stretching band (1620–1420 cm⁻¹) were normalized against the C-H alkanes stretching band (3000–2850 cm⁻¹) as an internal reference. The normalized intensity of the -OH band was observed to decrease progressively with increasing WT content, consistent with reduced oxygenated compound formation. Similarly, the C=O band intensity showed a marked reduction from pure GW100 to GW50+WT50 and further to pure WT, confirming the suppression of carbonyl-containing compounds. Conversely, the aromatic C=C band intensity increased with higher WT ratios, reflecting the enrichment of hydrocarbon structures in the pyrolysis products. These semiquantitative trends corroborate the chemical shifts observed in the GC-MS analysis and demonstrate the synergistic chemical bond evolution during co-pyrolysis.

The -OH free stretching bond at 3800–3500 cm⁻¹ indicates free alcohols, while C-H stretching in alkanes (3000-2850 cm⁻¹) confirms the presence of hydrocarbon chains. Aldehyde stretching (2830-2695 cm⁻¹) and CO₂ stretching (~2350 cm⁻¹) further support the oxygenated nature of biomass-derived oils, while C≡C bonds in alkynes (2260-2100 cm⁻¹) and C=C stretching in aromatic rings (1620–1420 cm⁻¹) indicate unsaturated hydrocarbons. Additionally, C-N and C-O stretching (1250-1020 cm-1) suggest aliphatic amines and oxygenated organic groups, whereas bending vibrations of alkenes and aromatics (1000-650 cm⁻¹) confirm structural characteristics of these compounds. The trans C-H bending (990-940 cm⁻¹), benzene ring C-H bending (900-675 cm⁻¹), and out-of-plane C-H bending in benzene (810-750 cm⁻¹) help determine aromatic substitution patterns, while sp² hybridized C-H bending (616-519 cm-1) is indicative of benzene and aromatic systems. This table serves as a crucial reference for interpreting FTIR spectra and characterizing hydrocarbons, oxygenated compounds, and aromatic structures present in the pyrolysis products of Gracilaria waste and waste tires.

3.3 Gas Chromatography-Mass Spectrometry (GC-MS)

A detailed chemical component analysis of the bio-oil was carried out using GC-MS. The compounds in the liquid product (bio-oil) were identified by comparing the chromatogram

Table 1 Functional chemical bond and wavelength range

No.	Functional bonds	Wavelength (cm ⁻¹)	Group
1	-OH free	3800-3500	stretching, free alcohol
2	C-H alkanes	3000-2850	stretching alkanes
3	H-C=O, C-H	2830-2695	stretching aldehydes
4	O=C=O	~2350	stretching CO ₂
5	-C=C- alkynes	2260-2100	stretching alkynes
6	C=C	1620-1420	Aromatic heteroatomic rings
7	C-N, C-O	1250-1020	stretching aliphatic amines and C-O stretching
8	=C-H	1000-650	bending alkenes
9	-C-H	990-940	bending trans RCH=CHR
10	C-H benzene	900-675	C-H aromatics benzene
11	-C-H	810-750	-C-H out of plane bending, m-subst., benzene
12	-C-H	790-650	-C-H bending cis RCH=CHR
13	С-Н	616, 519	C-H bending, alkene sp2 C-H aromatic sp2

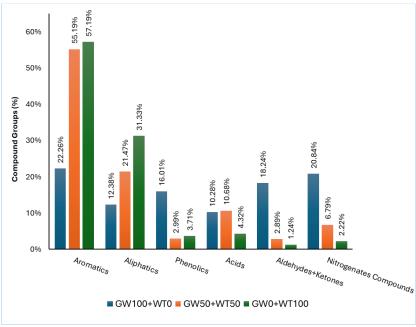


Fig. 6 The compound groups of bio-oil products

obtained from the standards. The pyrolysis bio-oil was a complicated mixture containing a wide range of chemical compounds.

Figure 6 shows GC-MS analysis of bio-oils with different mixture ratios of GW and WT content. Only the compounds with a relative similarity with the database higher than 60% are listed. It is observed that the liquid product contains many compound groups with different concentrations. Those compounds can be grouped as aromatics, aliphatics, phenolics, acids, aldehydes ketones, and nitrogenates compounds. Based on the three samples, bio-oil from GW100+WT0 contains more aromatics, aldehydes ketones, and nitrogenates compound groups. While bio-oil from GW50+WT50 and GW0+WT100 contains more aromatics and aliphatic compounds. Figure 6 also shows that the higher the WT ratio in raw materials, the higher the content of aromatic compounds in bio-oil products. Likewise, the aliphatic content in bio-oil will increase along with the increasing WT ratio in feedstock. This may be due to thermal instability and the breakdown of polymers and other long-chain compounds into smaller fragments during pyrolysis. The major chemical constituents of Gracilaria waste (GW) are carbohydrates, while waste tires (WT) contains many polymer compounds derived from petroleum. Accordingly, the major pyrolysis products and condensed bio-oil are derived from these components with different proportions depending on the feedstock mixture.

It is clear that the concentration of phenolics, aldehydes and ketones, and nitrogenates compounds in the bio-oil of both GW50+WT50 and GW0+WT100 was less than that for the bio-oil of pure Gracilaria (GW100+WT0). This can be attributed to the removal of oxygenated compounds during the addition of waste tire into Gracilaria. Adding WT to GW pyrolysis leads to a bio-oil with a different chemical composition. These compositional shifts can be explained by the underlying chemical mechanisms occurring during co-pyrolysis. The thermal cracking of waste tire polymers leads to random scission of C-C and C-H bonds, generating a high concentration of alkyl and hydrogen radicals (R• and H•). The presence of these radicals facilitates hydrogen transfer reactions that stabilize oxygenated intermediates derived from the biomass,

leading to a reduction in aldehydes, ketones, and phenolic compounds. Moreover, the H• radicals promote hydrodeoxygenation, converting oxygenated groups into water and hydrocarbons. In parallel, the scission of polymer chains from WT contributes to an increased formation of aromatic and aliphatic hydrocarbons, as detected in the GC-MS results. The synergistic effect between biomass and WT radicals thereby shifts the bio-oil composition toward higher hydrocarbon content while suppressing oxygenates and nitrogenates, consistent with the trends observed in our study. Similar radicalmediated mechanisms have been reported in co-pyrolysis systems by Tang et al. (2019) and Martínez et al. (2014c). It was evident that the hydrocarbon content was significantly increased with the addition of WT, and the relative contents of hydrocarbons increased as the WT share increased in the blends. Whereas an increase in WT content resulted in a decrease in nitrogenated and oxygenated compounds compared to pure GW biomass. When the WT percentage was 50%, the nitrogenate compounds were expectedly decreases from 20.84% to 6.79 %, and with pure WT (GW0+WT100) contains only 2.22% of nitrogenated compounds. Additionally, the aldehydes and ketones decrease significantly with the addition of WT50%, followed by pure WT100%. The decrease occurred from 18.24% in GW100+WT0 to 2.89% and 1.24% in GW50+WT50 and GW0+WT100, respectively. phenomenon is primarily due to the free radicals preventing amino acids from reacting with long-chain aliphatic acids to form amides (Kumar et al., 2022). This observation may be attributed to the interaction of H radicals derived from WT with the C=O double bonds of aldehydes or the C-CO bonds in ketones, consequently leading to CO generation (Tang et al., 2019).

A comparable advantageous impact of WT has been reported in prior research concerning various types of biomass. Alvarez *et al.* (2019) examined the co-pyrolysis process involving lignocellulosic biomass and waste tires, noting that adding waste tires significantly reduced the presence of oxygenated compounds while concurrently enhancing the synthesis of hydrocarbons. Sanahuja Parejo *et al.* (2018) reported an increase in the production of cyclic hydrocarbons

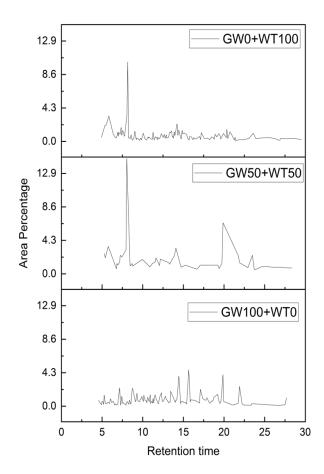


Fig. 7 The chromatograms of three bio-oil samples with various feedstocks

and reduce the phenolic compounds when waste tires were copyrolyzed with grape seeds. The presence of high carbon and hydrogen material promoted the decomposition of oxygenated compounds from biomass, inhibiting the generation of aldehyde, ketone, and furan groups (Yuan et al., 2018). Similarly, Martinez et al. observed that adding waste tires to the biomass pyrolysis decreased the amount of ketones, aldehydes, and phenolic compounds in the bio-oil (Martínez et al., 2014a). Figure 7 shows the chromatograms of three bio-oil samples by GC-MS method in spectrum mode. As seen in chromatograms, the samples showed different peak intensities in qualitative profiles. The results of peak identification are shown in Table A1, A2, and A3 for the three samples. These tables contain the compounds, retention times, and area percentages. The bio-oil derived from GW pyrolysis (GW100+WT0) exhibited relatively high nitrogenate compounds of 20.84% and oxygenated content of 34.25%. On the other hand, the bio-oil from WT pyrolysis (GW0+WT100) was characterized by a markedly lower presence of nitrogenate and oxygenate compounds (7.17%), with a significant content of hydrocarbon compounds (88.52%). We can conclude that adding WT to the GW prior to biomass pyrolysis increases the concentrations of hydrocarbon compounds (aromatics and aliphatic groups) in the bio-oil product.

4. Conclusion

This study highlights the potential of co-pyrolyzing Gracilaria waste (GW) and waste tires (WT) to enhance bio-oil properties, particularly by improving hydrocarbon content and reducing

oxygenated compounds. The thermogravimetric analysis (TGA) results demonstrated that the thermal degradation of the mixture shifted towards higher temperatures, indicating improved thermal stability. The Fourier Transform Infrared Spectroscopy (FTIR) analysis revealed significant transformations in chemical bonds, with a decrease in hydroxyl (-OH) groups and an increase in hydrocarbon-related bonds (C-H, C=C, and C-C), which contribute to the improved fuel quality of the liquid product. These findings contribute to the broader field of biomass conversion and waste valorization by demonstrating the synergistic effects of co-pyrolysis between marine biomass and polymeric waste. The study provides valuable insights into the chemical interactions that occur during co-pyrolysis, offering a feasible approach to optimizing bio-oil composition for potential applications in renewable energy and sustainable waste management. Further research should explore the influence of reaction conditions, such as catalyst addition and temperature variations, on product composition and yield. Additionally, the long-term stability and upgradability of the derived bio-oil should be assessed to facilitate its practical implementation in energy applications.

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Author Contributions: I.M.: Conceptualization, preparation of equipment and materials, collection of experimental data, data analysis, writing the original draft of manuscript, S.E.M.; supervision, resources, and review, D.A.S.; monitoring, review and editing, project supervision, and validation, A.A.; manuscript review, editing, and validation, W.J.Y.; supervision, manuscript review, and validation. All authors have read and agreed to the published version of the manuscript.

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Appendix

Table A1. The GC-MS analysis of bio-oil GW100+WT0 pyrolysis

1.92 0.55 0.35 4.03 0.35 0.15 0.96 0.60 0.27 0.64 0.77
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0.47
0.64
0.41
0.15
0.64
0.13
0.84
0.61
1.02
0.42
3.87
0.51
1.17
1.53
0.62
0.58
0.18
2.55
0.26

Heptadecane

Compounds	R.T.	%	Compounds	R.T.	%
Aromatics and Benzene derivatives			Tricosane	22.94	0.80
Ethylbenzene	5.26	2.62	Tetracosane	23.79	0.5
Benzene, 1,3-dimethyl-	5.40	2.06	Pentacosane	24.59	0.9
Benzene, propyl-	6.77	0.65	Hexacosane	25.36	0.9
Benzene, 1-ethyl-4-methyl-	6.94	1.12	Heneicosane	26.10	0.8
AlphaMethylstyrene	7.24	2.37	Nonacosane	26.84	0.8
o-Cymene	7.94	3.09	Heptacosane, 1-chloro-	27.55	0.7
D-Limonene	8.03	14.79			
o-Cresol	8.70	1.32	Phenolics		
H-Indene, 1-methyl-	9.95	1.85	Phenol	7.15	1.4
Benzothiazole	11.16	1.28	Phenol, 3-methyl-	8.75	1.0
H-Indene, 1,3-dimethyl-	11.55	1.56			
H-Indene, 1,1-dimethyl-	11.62	2.06	Acids		
Benzene, 1-cyclopenten-1-yl-	12.17	1.90	n-Hexadecanoic acid	19.88	6.5
Biphenyl	13.31	1.24	Octadecanoic acid	21.76	2.3
Naphthalene, 2,7-dimethyl-	13.90	2.38			
Quinoline, 1,2-dihydro-2,2,4- rimethyl-	14.08	3.30	Aldehydes & Ketones		
Naphthalene, 1,6,7-trimethyl-	15.28	1.12	Benzenepropanal	8.45	1.0
Benzene, 1,1'-(1,3-propanediyl)bis-	16.69	0.60	Octahydrodipyrrolo, 10-dione	19.75	1.3
GammaElemene	19.40	0.68			
			Nitrogenates Compounds		
Aliphatics			2-(Methylthio)phenyl isothiocyanate	16.17	0.7
1,3,5,7-Cyclooctatetraene	5.75	3.52	Hexadecanenitrile	19.24	1.1
,5-Cyclooctadiene, 1,5-dimethyl-	6.83	1.34	Hexadecanamide	21.92	1.4
cis-2,6-Dimethyl-2,6-octadiene	7.45	2.17	1,4-Benzenediamine, N-(1,3-dimethylbutyl)	23.48	2.4
Гridecane	12.06	1.06	Octadecanamide	23.70	0.7
1,2,3-Trimethylindene	13.20	1.43			
Pentadecane	14.71	0.86			
** . 1					

17.08

1.13

Compounds	R.T.	%	Compounds	R.T.	%
Aromatics and Benzene derivatives			Cyclohexene, 1-methyl-4-(1-methylethenyl)	7.79	0.86
Ethylbenzene	5.35	2.06	p-Mentha-1,5,8-triene	8.56	0.85
p-Xylene	5.49	2.08	Cyclohexene, 1-methyl-4-(1-	9.04	1.32
Styrene	5.84	3.25	methylethylidene)- Undecane	9.20	0.25
Benzene, (1-methylethyl)-	6.37	0.94	Cyclohexene, 3-methylene-4-(1,2-	9.48	0.33
Benzene, 1,1'-(1-ethenyl-1,3-			propadienyl)- 7-Ethylidenebicyclo[4.2.1]nona-2,4-		
propanediyl)bis-	6.73	0.45	diene	9.66	0.24
Benzene, propyl-	6.86	0.75	Cyclooctene, 3-(1-methylethenyl)-	9.73	0.42
D-Limonene	6.94	1.18	Bicyclo[2.2.1]heptane, 2,2-dimethyl-3-methylene	9.86	0.22
Benzene, 1-ethyl-4-methyl-	6.99	0.67	Cyclopropylphenylmethane	10.26	0.3
Benzene, 1-ethyl-3-methyl-	7.04	1.15	Dodecane 5H-Benzocycloheptene,6,7,8,9-	10.73	0.4
Aniline	7.23	0.93	tetrahydro-	11.21	0.30
Alpha Methylstyrene	7.34	1.81	Bicyclo[6.4.0]dodeca-9,11-diene	11.66	0.5
p-Cymene	8.06	3.46	Tridecane 8,9-Dimethylbicyclo[4.4.1]undeca-	12.18	0.62
D-Limonene	8.16	10.21	2,4,8-triene	13.11	0.52
Indane	8.25	0.46	Tetramethylbicyclo[7.2.0]undeca-2,6-	13.17	0.53
Benzene, 1-propynyl-	8.41	0.43	diene Tetradecane	13.54	1.3
Benzene, 1-propyllyi- Benzene, 1-methyl-2-propyl-	8.46	0.43	Cyclohexene, 4-(2-bromoethyl)-	13.88	1.2
Benzeneacetaldehyde, .alphamethyl-	8.71	0.16	Valerena-4,7(11)-diene	13.96	0.7
p-Cymene	8.90	0.41	Quinoline, 2,4-dimethyl-	14.22	2.2
Benzene, 1-methyl-4-(1- methylethenyl)-	9.10	0.75	1-Pentadecene	14.74	0.3
Benzene, 1-methyl-4-(1-	0.42	0.22	Donto do como	14.04	1.4
methylpropyl)-	9.42	0.32	Pentadecane	14.84	1.4
6,7-Dimethyl-3,5,8,8a-tetrahydro-1H- 2-benzopyran	9.58	0.15	1,5-Cyclodecadiene	14.93	0.9
1H-Indene, 2,3-dihydro-5-methyl-	9.91	0.47	Guaia-9,11-diene	15.57	0.3
1H-Indene, 1-methyl-	10.06	1.06	Cetene	15.96	0.6
Benzene, pentyl-	10.14	0.81	2-Bromo dodecane	16.05	0.5
Benzene, 2-ethenyl-1,3,5-trimethyl- 1H-Indene, 2,3-dihydro-1,2-dimethyl-	10.46 10.62	0.17 0.50	3-Heptadecene Heptadecane	17.12 17.21	0.2 1.1
			1-Cyclohexene-1-butanol, 2,6,6-		
Naphthalene	10.65	0.59	trimethyl-	18.23	0.2
1H-Indene, 2,3-dihydro-1,2-dimethyl-	10.77	0.54	Hexadecane	18.29	0.3
Benzene, 2-ethenyl-1,3,5-trimethyl- Benzothiazole	11.12 11.26	0.27 1.19	1,3,6,10-Cyclotetradecatetraene Cyclohexane, 1-ethenyl-1-methyl	18.72 19.53	0.4
Benzene, 1-cyclopenten-1-yl-	11.40	0.20	Eicosane	20.35	1.5
Benzene, cyclohexyl-	11.55	0.60	Heptane, 1,7-dibromo-	20.46	0.3
Naphthalene, 1,2-dihydro-3-methyl-	11.72	0.49	2-Dodecen-1-yl(-)succinic anhydride	21.29	0.1
1H-Indene, 1,1-dimethyl-	11.79	0.22	Bisnorabieta-5,7,9(10),11,13-pentaene	21.43	0.0
Naphthalene, 1,2-dihydro-3-methyl-	11.84	0.56	Heptadecane	22.20	0.2
1H-Indene, 2,3-dihydro-1,2-dimethyl- Naphthalene, 1-methyl-	12.01	0.33	Tricosane Tetracosane	23.07	0.3
Naphthalene, 1-methyl-	12.28 12.52	1.01 0.50	Heptacosane	23.91 24.72	0.3
Benzene, 1,3,5-trimethyl-2-(1-		0.91	•		
methylethenyl)-	12.64		Hexacosane	25.49	0.4
Benzene, 3-cyclohexen-1-yl-	12.77	0.41	Nonacosane	26.23	0.3
Benzene, 1-butyl-4-methoxy- 1,2,3-Trimethylindene	12.96 13.31	0.44 1.19	Triacontane Tetratriacontane	28.54 29.50	0.4
Naphthalene, 1,2-dihydro-3,5,8-	13.72	0.65	Tetratriacontaile	23.50	0.2
trimethyl-	13.72	0.05			
Naphthalene, 1,2,3,4,4a,5,6,8a- octahydro-4a,8-dimethyl	13.77	0.42	Phenolics		
Naphthalene, 2,7-dimethyl-	14.02	1.14	4-Chloro-3-ethylphenol	13.64	0.6
Alloaromadendrene	14.32	0.78			
	4 4 40	1.46	Acids		
4,7-Dimethyl-1,2,3,4,4a,5,6,8a- octahydronaphthalene	14.43	1.40	110103		
	14.43 14.66	0.51	9,12-Octadecadienoic acid	7.41	0.78

Compounds	R.T.	%	Compounds	R.T.	%
Naphthalene, 1,4,6-trimethyl-	15.62	0.32	m-Anisic acid, pent-2-en-4-ynyl ester	16.14	0.25
Alloaromadendrene	15.71	0.19	1H-Thieno[3,4-d]imidazole-4- propanoic acid	16.99	0.63
Alloaromadendrene	15.75	0.61	Octadecanoic acid	21.83	0.23
Benzene, [1-(2,4-cyclopentadien-1- ylidene)ethyl]-	16.22	0.30	Octadecanoic acid, ethyl ester	22.13	0.23
Fluorene, 2,4a-dihydro-	16.27	0.48			
Naphthalene, 1-(1,1-dimethylethyl)-	16.41	0.32	Aldehydes & Ketones		
Benzene, 1,1'-(1,3-propanediyl)bis-	16.80	0.52	6-Methyl-5,6,7,8-tetrahydro-2,4- quinazolinedione	17.46	0.63
Benzene, (4,5,5-trimethyl-1,3- cyclopentadien-1-yl)-	17.56	0.39	Pregn-17(20)-en-16-one	18.77	0.27
Benzene, 1,1'-(1,4-butanediyl)bis-	17.95	0.44	Androstan-17-one	19.59	0.31
Naphthalene, 2-(1-cyclopenten-1-yl)-	18.47	0.58			
Retene	22.54	0.25	Nitrogenates Compounds		
Phenantrene-9,10(9H,10H)	26.86	0.15	Nicotinonitrile, 1,4-dihydro-1-propyl-	9.27	0.43
			Hexadecanenitrile	19.35	1.00
Aliphatics			Octadecanenitrile	21.35	0.54
Cyclohexene, 4-ethenyl-	4.92	0.52	4-Amino-6-iodo-1-methyl-3-oxo-7-carbonitrile	26.63	0.20
1,3,6-Heptatriene, 2,5,6-trimethyl-	6.67	0.47			
cis-2,6-Dimethyl-2,6-octadiene	7.55	1.42			
7-Methylenebicyclo[4.2.0]octane	7.74	0.65			